

Technology Development for Carbon Capture and Conversion



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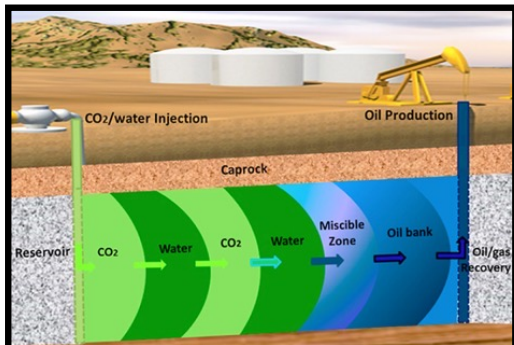
Dan F. Smith Department of Chemical
& Biomolecular Engineering



The Tale of Two Terms

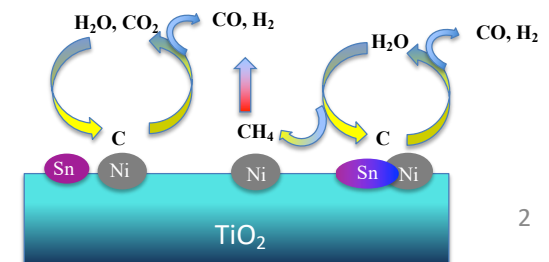
Near Term

- **Carbon Capture**
 - Higher CO₂ comp streams
 - Amine absorption
- **Carbon Utilization**
 - Enhanced Oil Recovery



Longer Term

- **Carbon Capture**
 - Lower CO₂ comp streams
 - Ionic Liquid absorption, pressure swing adsorption
- **CO₂ Conversion**
 - Tri-reforming
 - Photocatalytic conversion



The Disclaimer:

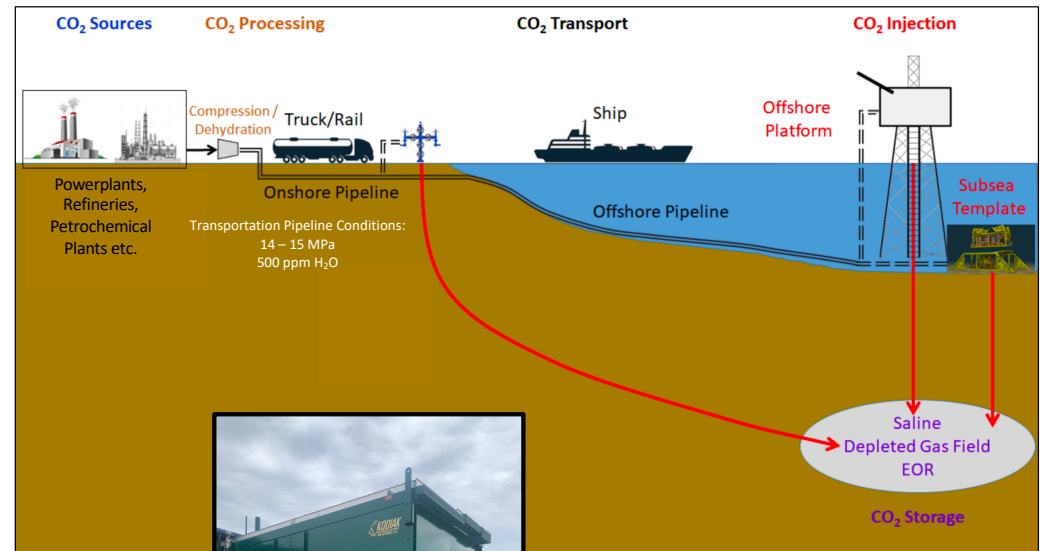
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Carbon Capture and Storage (CCS)

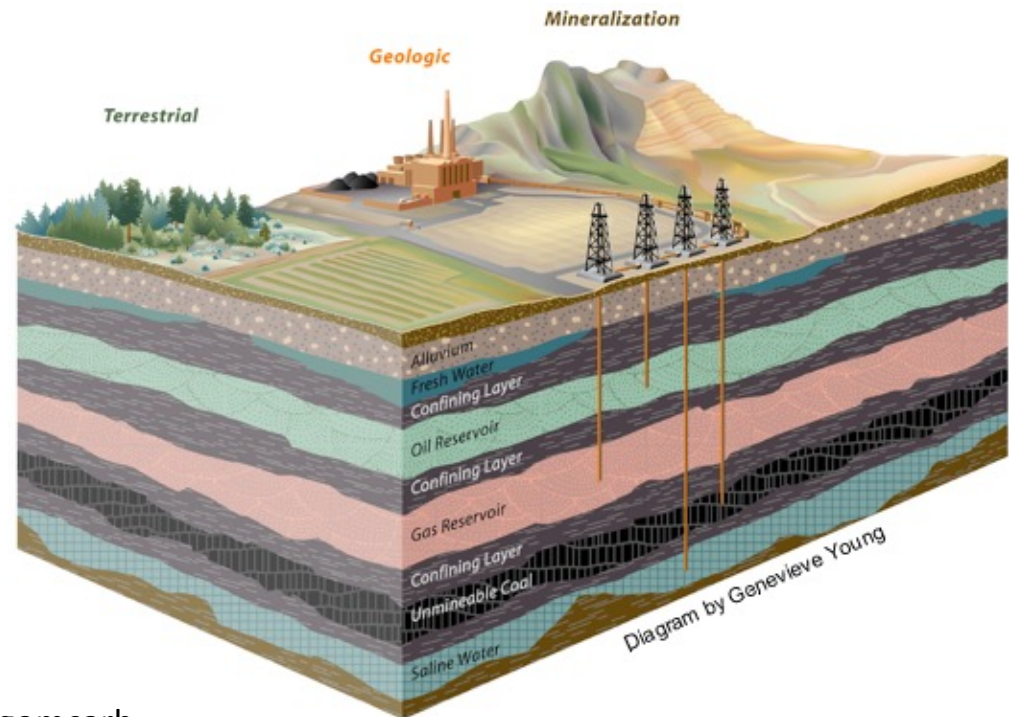


Deep Underground Storage

Gulf of Mexico Partnership for Offshore Carbon Storage (GoMCarb)

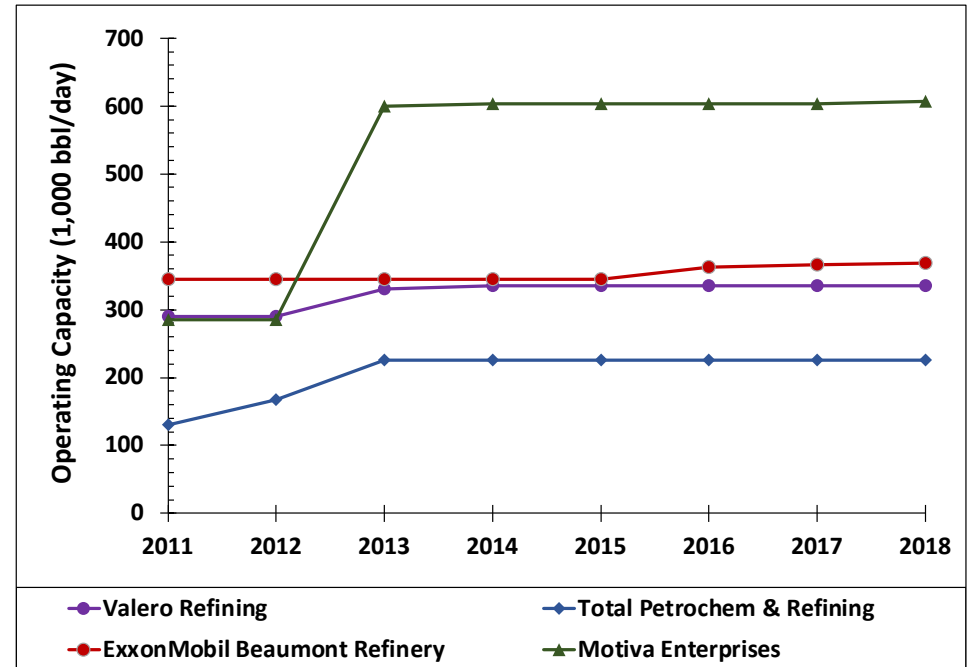
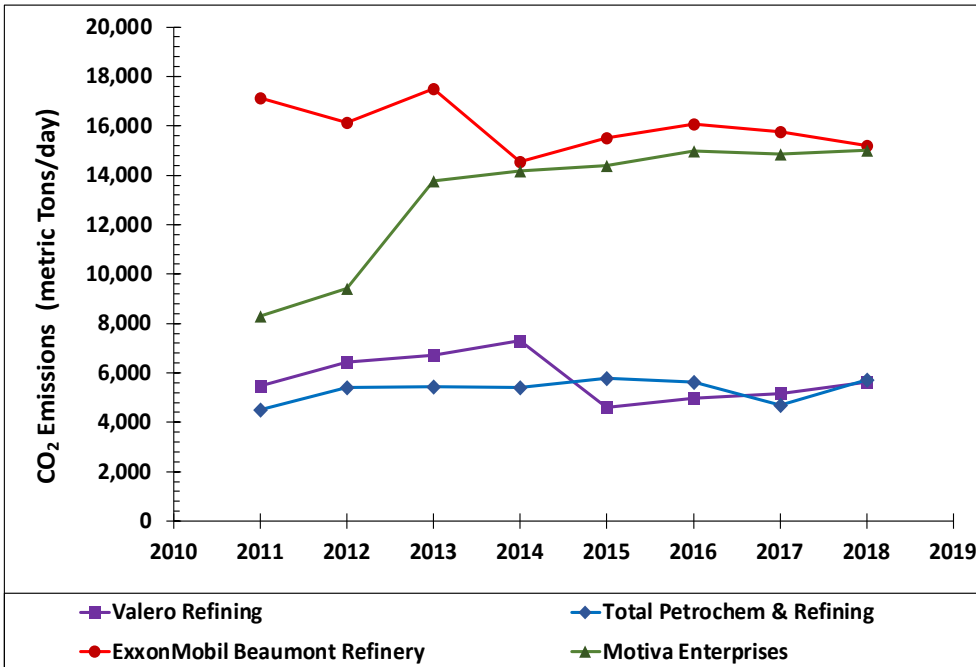
Why Store in Gulf of Mexico?

- Well studied geology
- Industrial CO₂ emission sources
- Large volume, low risk
- Industrial sources close to transportation facilities
- Existing Capture and transportation
- Commercial EOR to offset costs



<http://www.beg.utexas.edu/gcc/research/gomcarb>

Evaluation of Annual CO₂ Emissions from Refineries



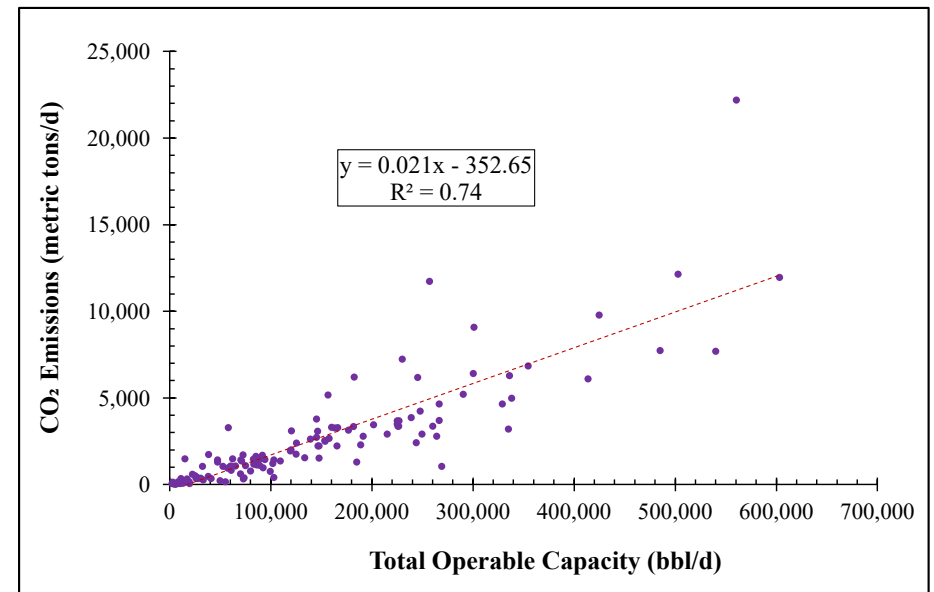
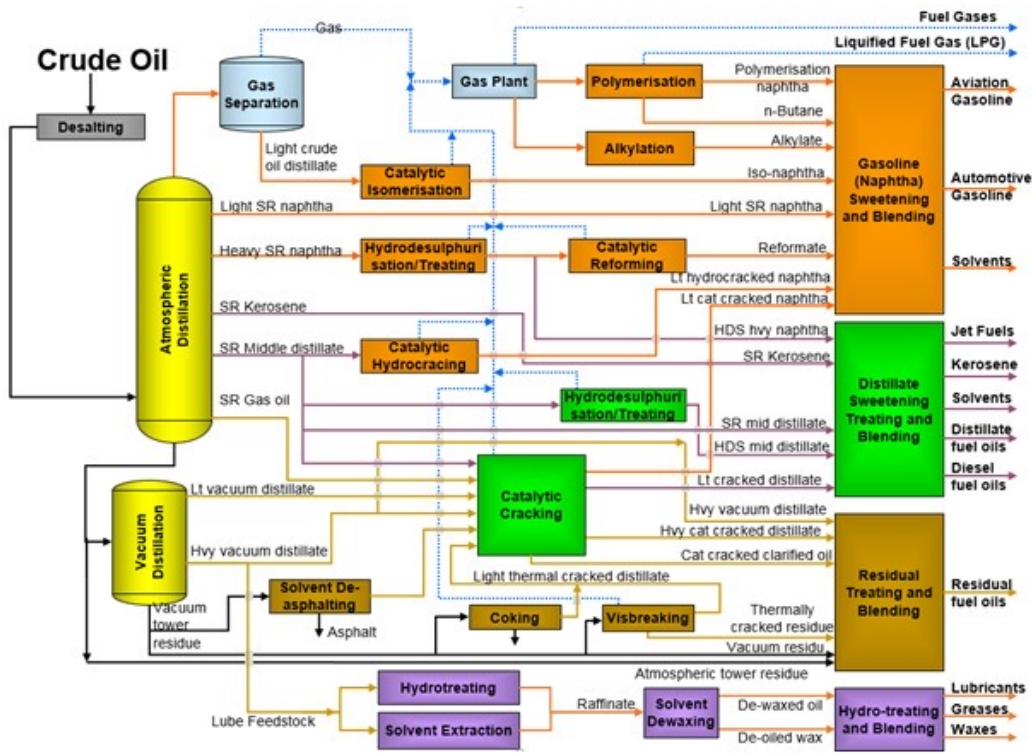
Data Sources:
 Refinery Capacity Report,
 U.S. Energy Information Administration



Data Sources:
 FLIGHT
 United States Environmental Protection Agency



CO₂ Emissions vs Operating Capacity



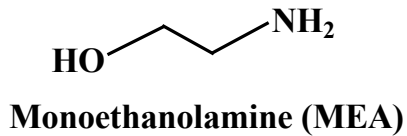
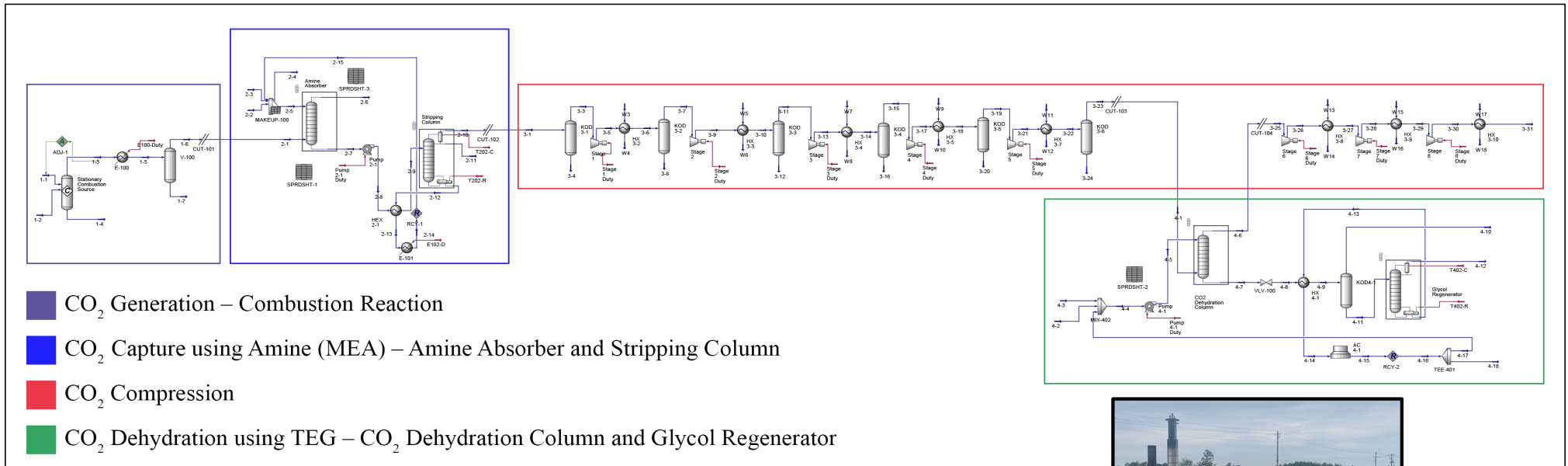
Carbon Capture and Storage (CCS)

(Process simulation from waste flue gas to pipeline quality)

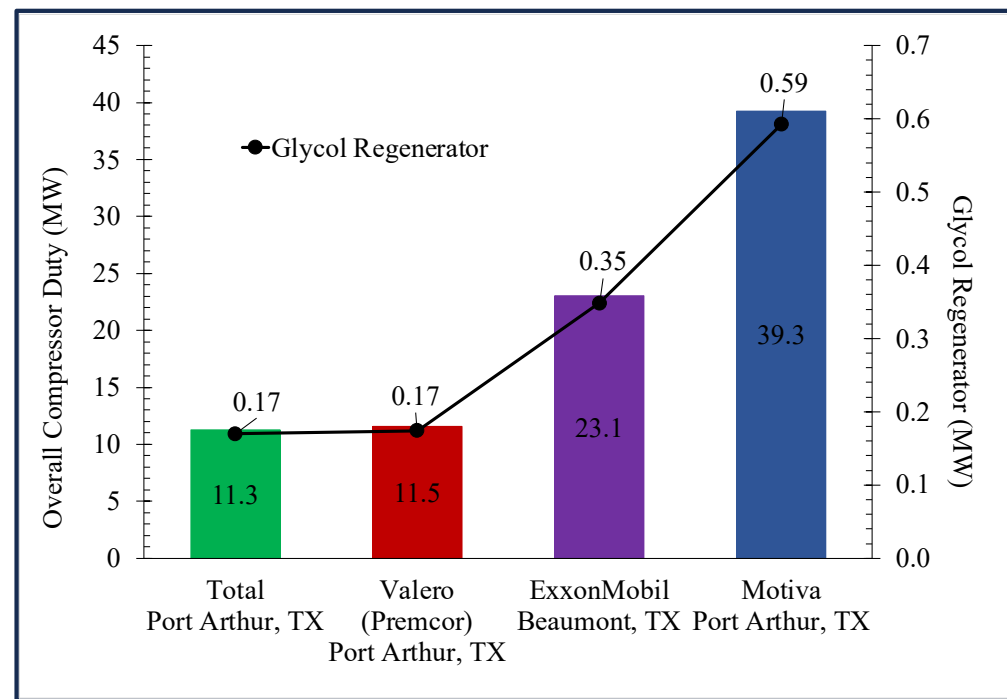
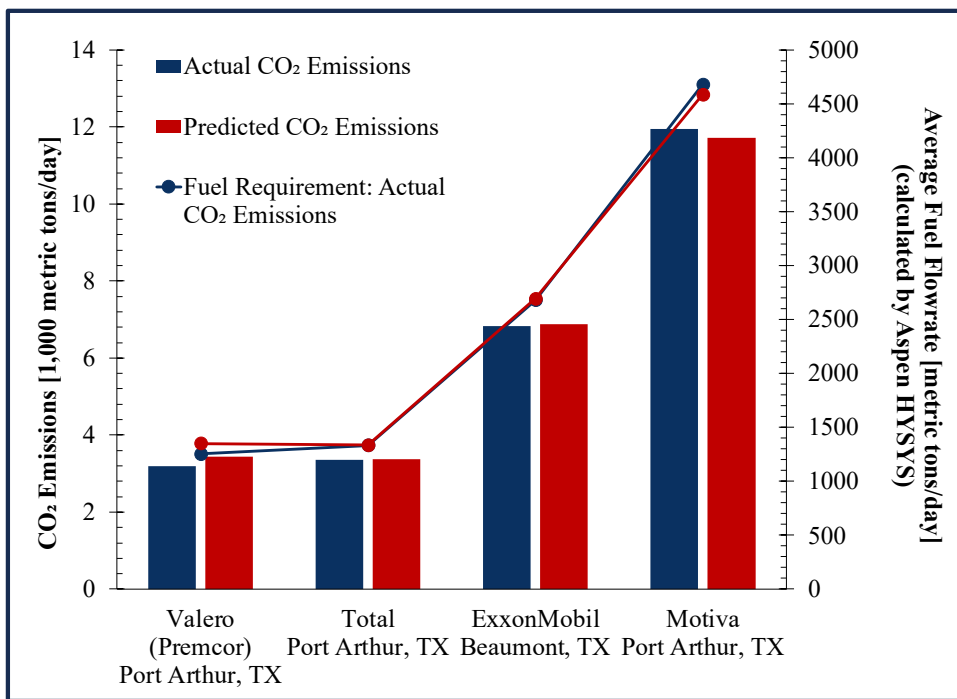
10 – 15 wt% CO₂ and 1 atm



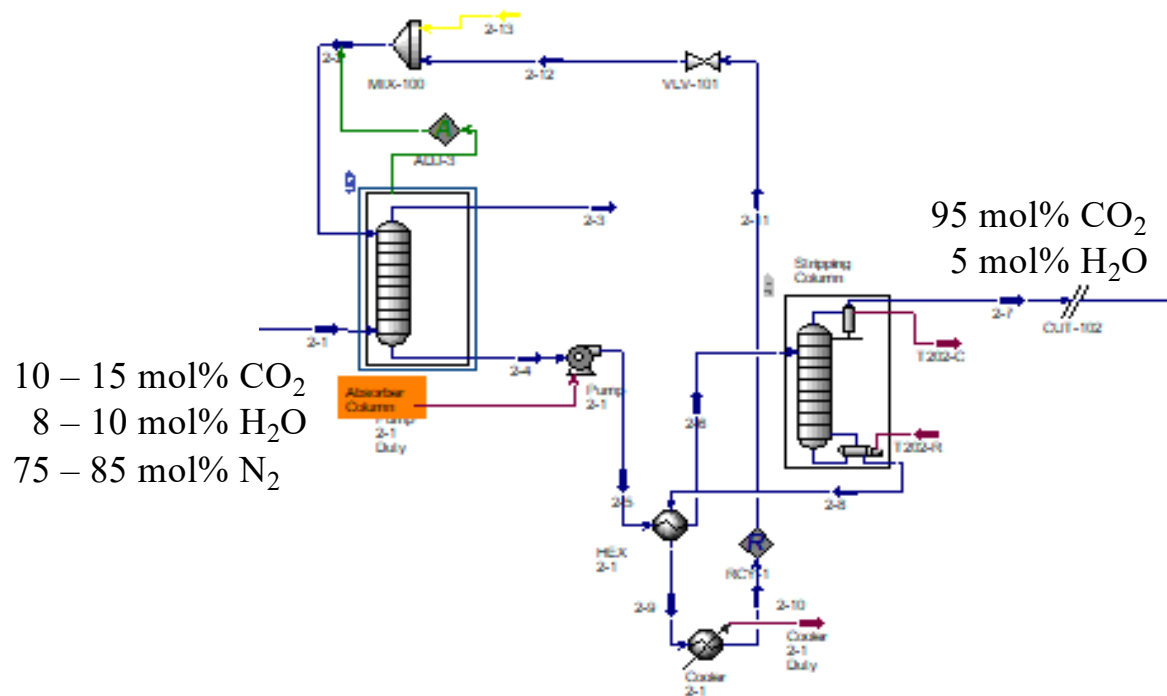
CO₂ w/ 500 ppm water and 130 atm



Process Simulation: Actuals vs Predicted



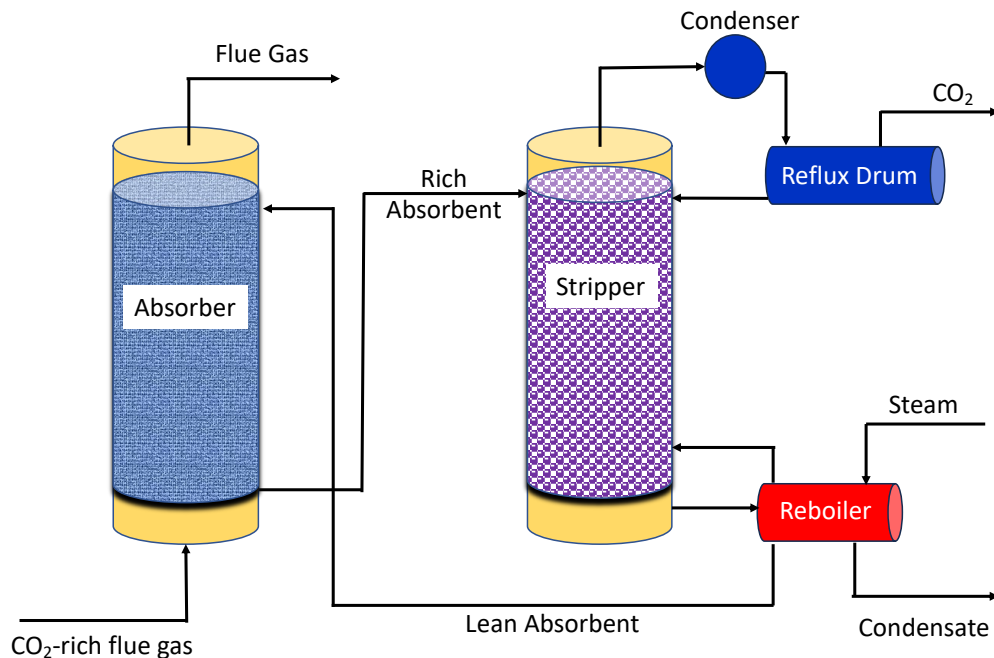
Carbon Capture Using Cyclic Absorption/Stripping



Amine Absorbents

- + Established chemistry
- + Established technology
- + Industry ready
- High energy demand
- Amine degradation
 - Temperature
 - O₂, SO_x, NO_x

Capturing of Flue Gases (10 – 15 wt% CO₂)



❖ Amines

- ❖ Current Technology

- ❖ High regeneration costs

- ❖ Produces VOCs

- ❖ Poisoned by contaminants

❖ Ionic Liquids

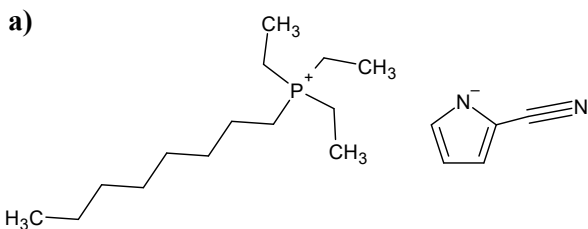
- ❖ Lower regeneration costs

- ❖ No VOCs

- ❖ High viscosities

- ❖ Poisons (??)

Aprotic Heterocyclic Anion Ionic Liquids (AHA-IL)

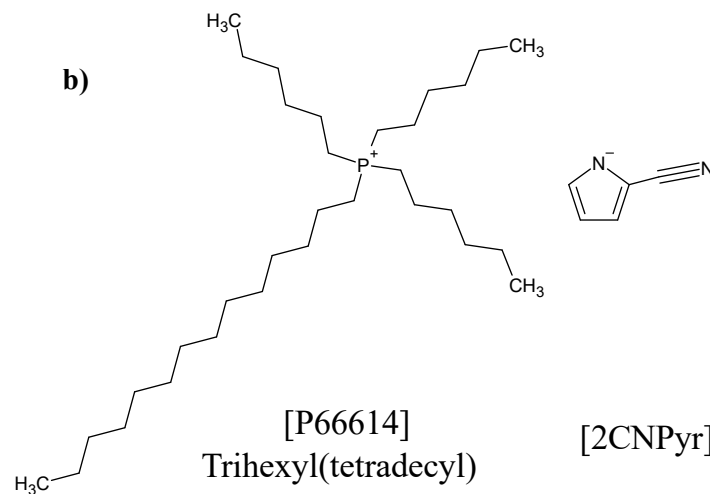


[P2228]

Triethyl(octyl)
phosphonium

[2CNPyr]

2-Cyanopyrrolide



[P66614]

Trihexyl(tetradecyl)
phosphonium

[2CNPyr]

2-Cyanopyrrolide

Henry's Law:

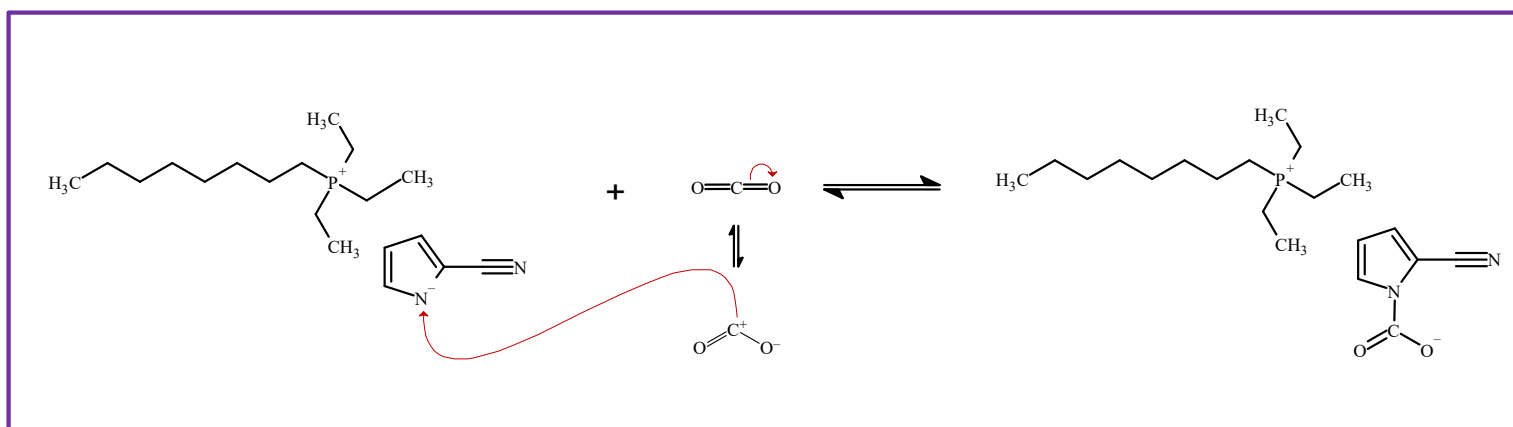
$$P_{\text{CO}_2} = y_{\text{CO}_2} P = x_{\text{CO}_2} H(T)$$

Viscosity \uparrow , Diffusivity \downarrow
Temperature \uparrow , Viscosity \downarrow
Temperature \uparrow , Capacity \downarrow



FreakingNews.com

Chemisorption Mechanism

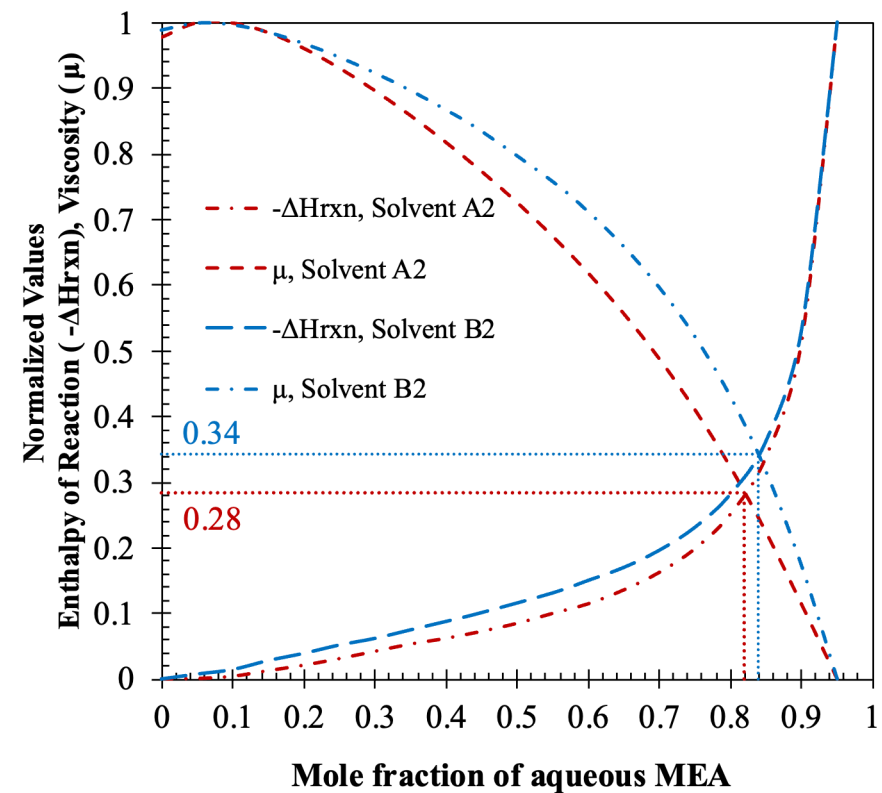
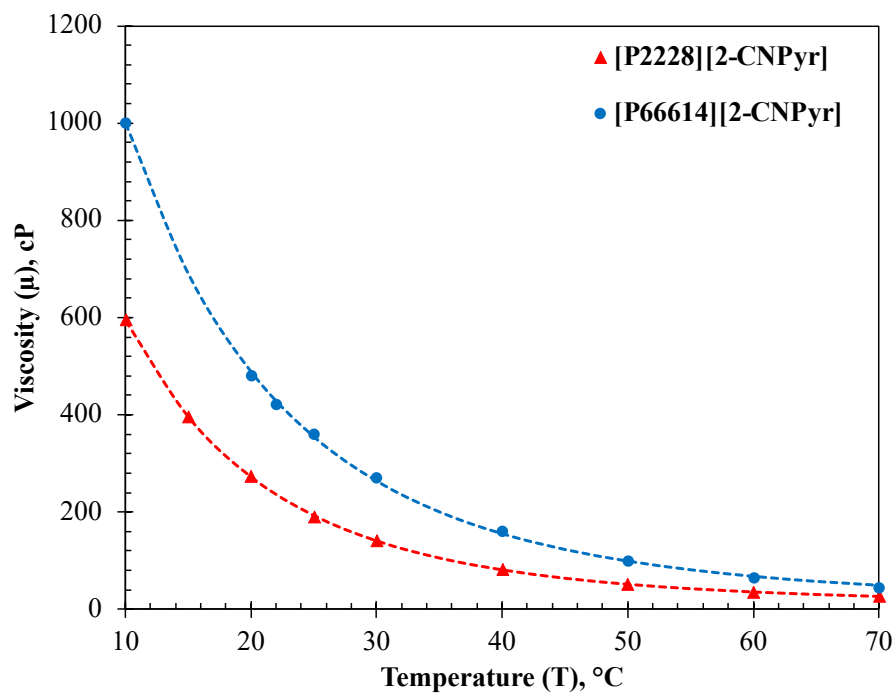


$$\ln(K_H) = A_{H,i} + \frac{B_{H,i}}{T}$$

$$\ln(K_{eq}) = A_{K,i} + \frac{B_{K,i}}{T}$$

$$\ln(K_{eq}) = \frac{\Delta S}{R} + \left(\frac{-\Delta H_{chem}^0}{RT} \right)$$

IL/MEA Hybrid Solvent



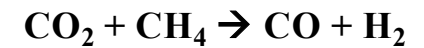
Solvent A: [P2228][2-CNPy]
Solvent B: [P66614][2-CNPy]

CO₂ - Birth, Death, and Reuse

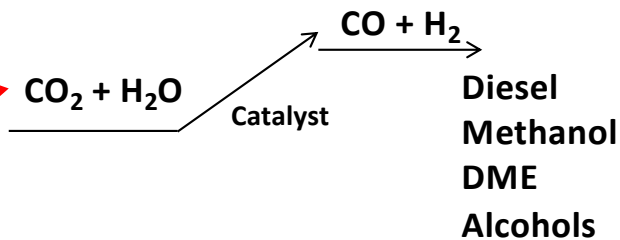
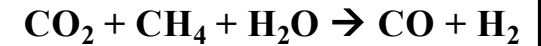


Thermo-Chemical

✓ Dry Reforming

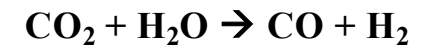


✓ Tri-Reforming



Non-thermo-Chemical

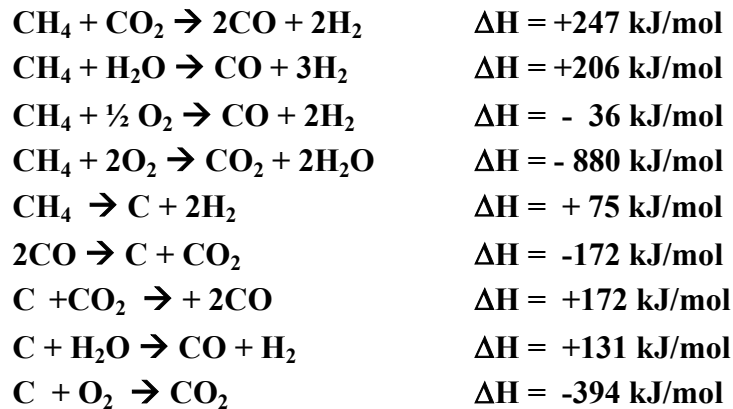
✓ Electrolytic



✓ Photocatalytic

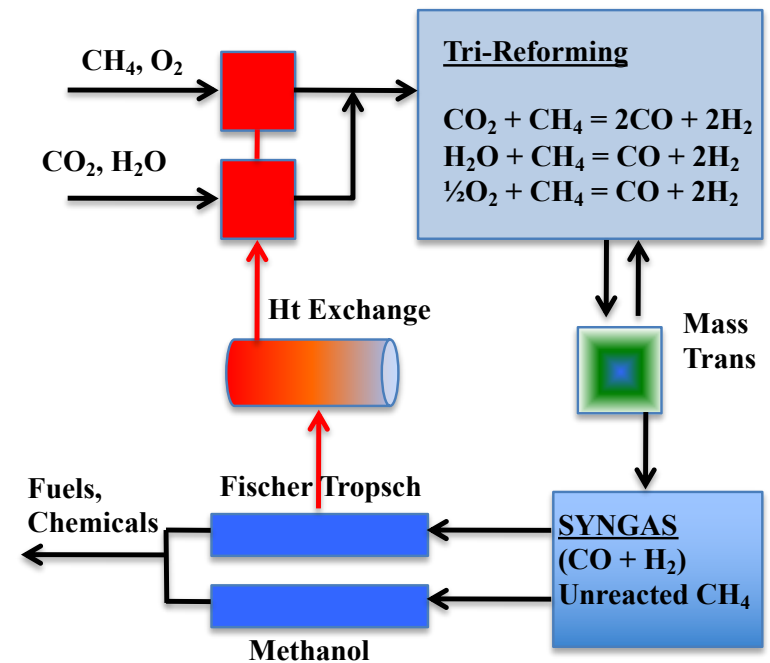


Tri-Reforming: Turning CO₂ into a Fuel



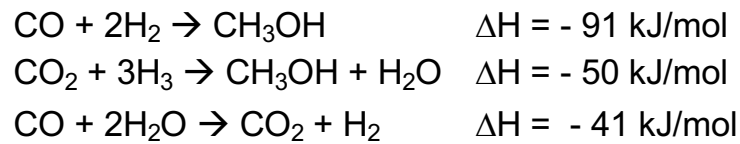
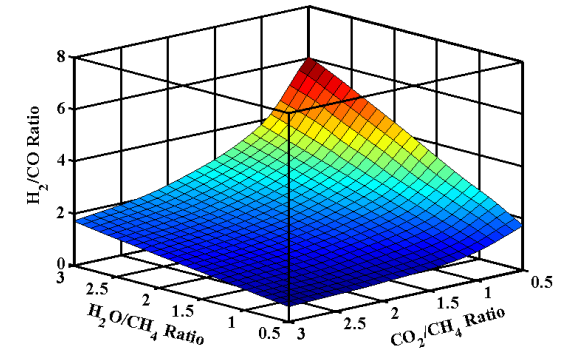
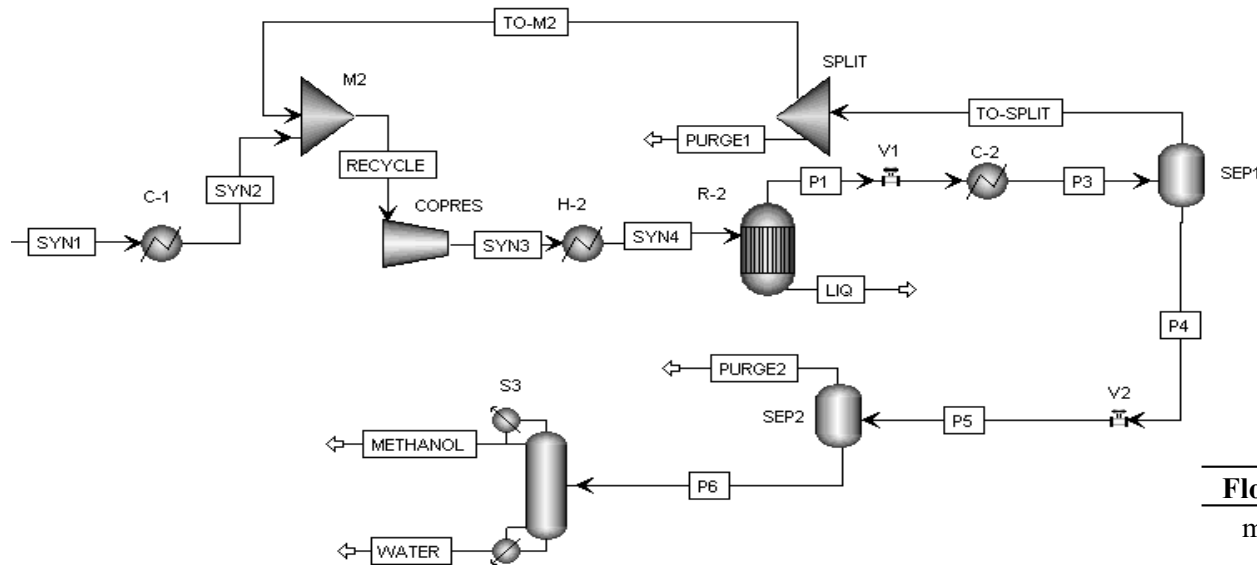
Conversion: 70% CO₂, 98% CH₄
 H₂/CO = 1.5 – 2.0

- Conversion and utilization of CO₂ without CO₂ separation from power plant
- Effective production of syngas with desired H₂/CO ratio for Fischer –Tropsch synthesis
- Reducing the possibility of carbon formation compared with dry reforming



Zhang et al. (2013) Int. J H₂ Energy, 38, 13617-13630.
 Zhang et al. (2014) Energy & Fuels, 28, 2717-2726.
 Zhang et al. (2014) Chem Eng & Tech, 37, 1493-1499.
 Zhang et al. (2015) Fuel Proc Tech, 131, 37-46

Combined Methanol Synthesis and Tri- Reforming

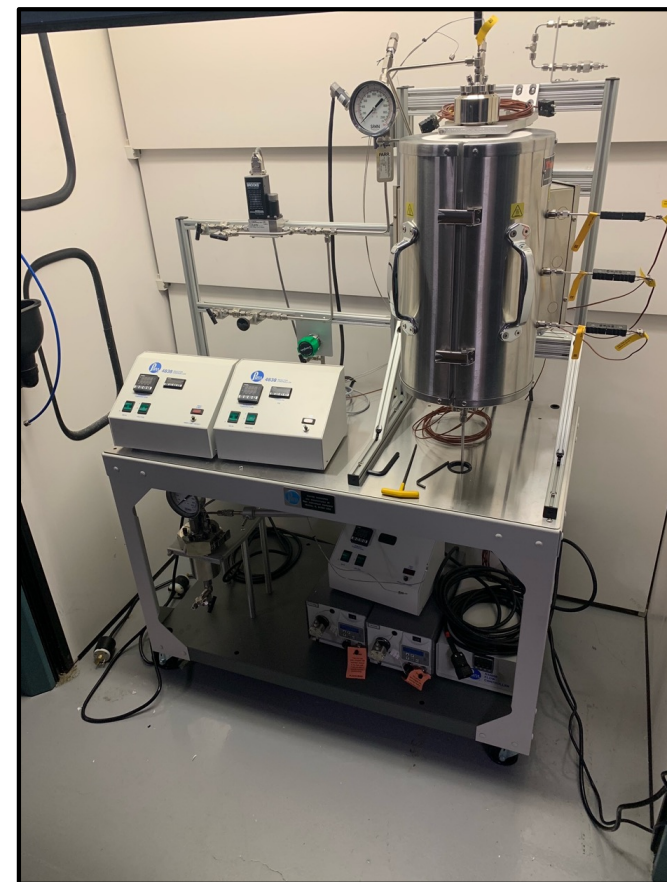


Flowsheet Element	Parameter	Value
methanol reactor	temperature (°C)	220
	pressure (bar)	50
sep1	temperature (°C)	25
	pressure (bar)	24
sep2	temperature (°C)	25
	pressure (bar)	10
S3 (Radfrac)	Number of stages	19
	Feed stage	11
	Reflux ratio	1.5
	Distillate to feed ratio	0.988

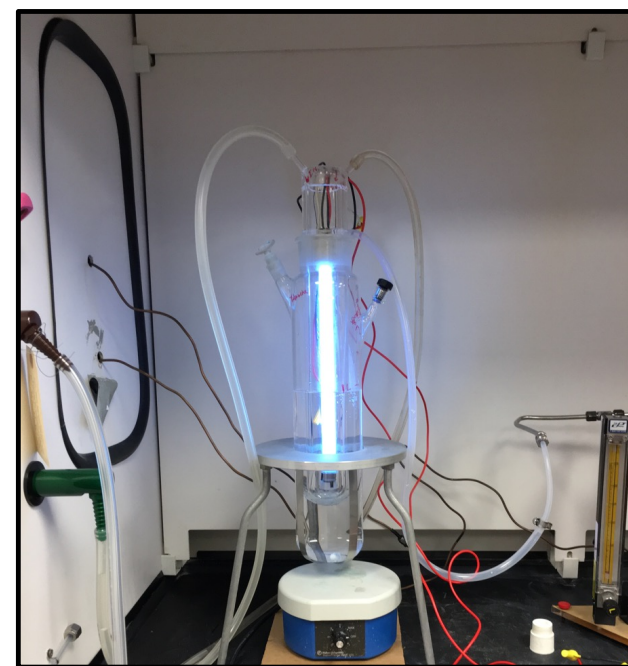
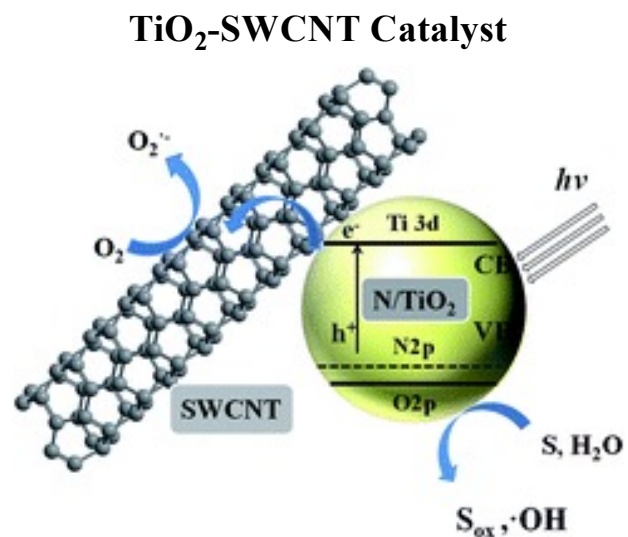
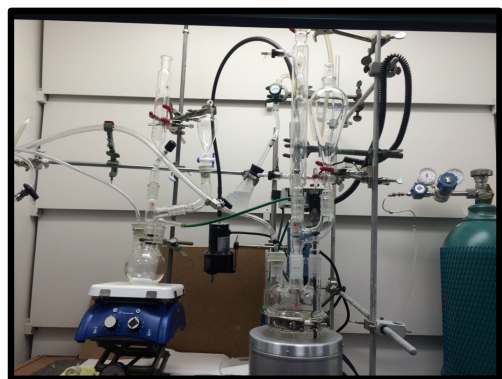
Tri-Reforming – Searching for the Right Catalyst

Catalyst	Reaction Conditions	% Conversions (H ₂ :CO ratio)	H ₂ :CO Ratio
Ni/MgO	850°C, 1 atm	75% CO ₂ , 95% CH ₄	1.5
Ni/MgO/CeZrO	850°C, 1 atm	70% CO ₂ , 93% CH ₄	1.6
Ni/Mg _x Ti _{1-x} O	700-850°C, 1 atm	75% CO ₂ , 98% CH ₄	2.0
NiO/YSZ/CeO ₂	650-850°C, 1 atm	100% CO ₂ , 90% CH ₄	1.67
Ni/Ce/ZrO ₂	750°C, 3 atm	80% CO ₂ , 88% CH ₄	1.2
Ni/SiO ₂	750°C, 1 atm	91% CO ₂ , 31% CH ₄	2.0
Ni-Mg/β-SiC	750 °C, 1 atm	50% CO ₂ , 75% CH ₄	1.5 – 2.0

- Need data under real conditions
- Catalyst and contaminants (NO_x/SO_x)



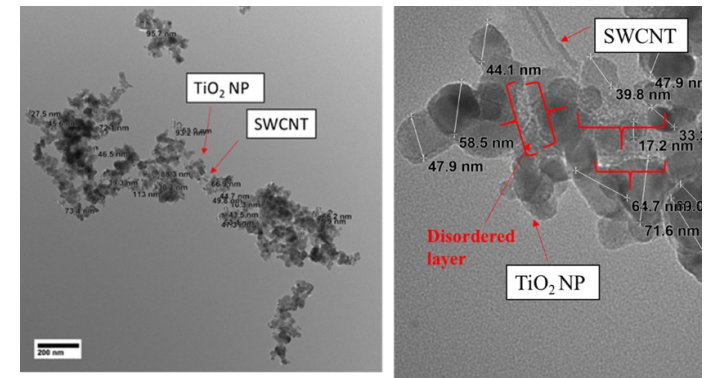
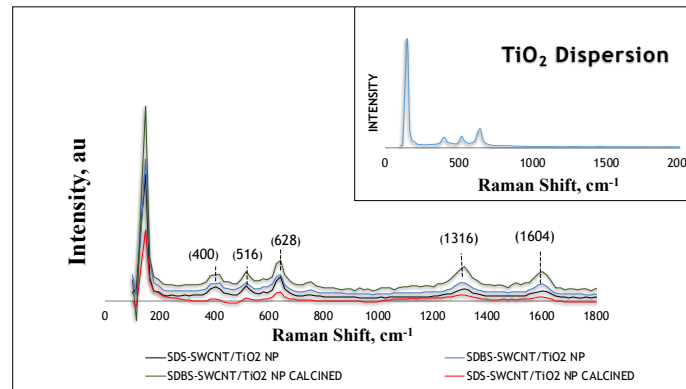
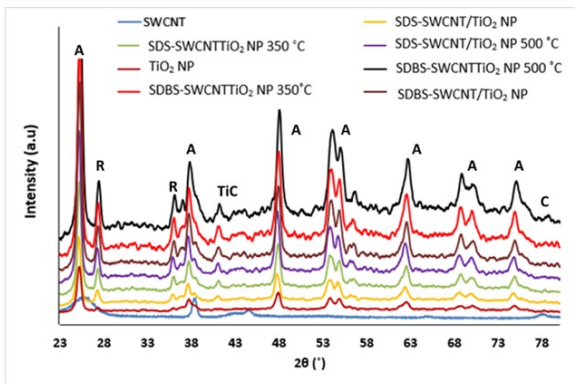
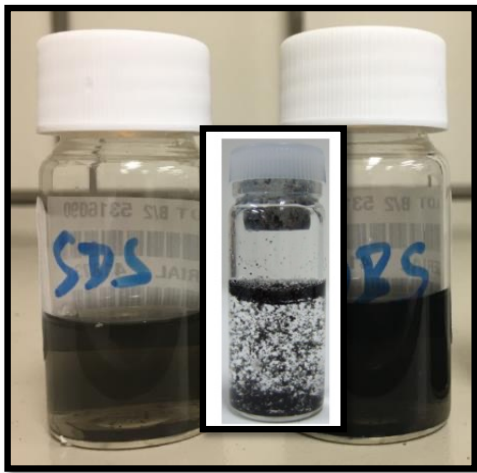
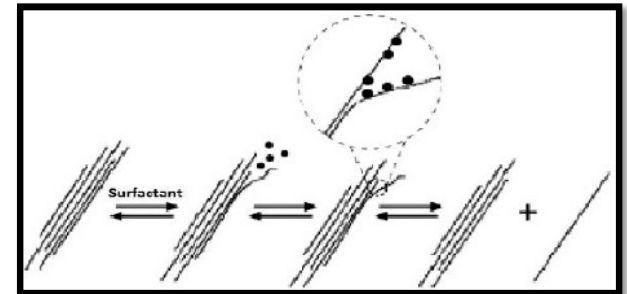
Photocatalytic Conversion of CO₂



Piler et al. (2020) Mater. Letters, 278, 12810
Piler et al. (2020) Adv Catal., 66, Ch. 2

TiO₂ – SWCNT Photocatalyst

- Band gap reduction
- Longer electron – hole pair separation
- Enhanced adsorption of reactants (Such as CO₂, H₂O)



Acknowledgements

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Dr. James Henry
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